IN THE CLAIMS:

The pending claims are set forth below and have been amended and/or cancelled, without prejudice, where noted:

1. (Currently Amended) A process for converting a carbon containing~~hydrocarbon~~ feedstock to provide an effluent containing light olefins, the process comprising passing a ~~hydrocarbon~~ feedstock containing carbon containing compounds consisting essentially of ~~at least one~~ C_1 to C_6 aliphatic hetero compounds selected from the group consisting of alcohols, ethers, carbonyl compounds and mixtures thereof and containing steam in an amount up to 80 weight % of said feedstock, through a reactor containing a crystalline silicate catalyst to produce an effluent including propylene which is recovered from the reactor, wherein the crystalline silicate catalyst is pretreated by subjecting said catalyst to steaming to de-aluminate said catalyst and is selected from at least one of an MFI-~~type~~ crystalline silicate having a silicon/aluminum atomic ratio within the range of 250 to 500 and an MEL-~~type~~ crystalline silicate having a silicon/aluminum atomic ratio within the range of 150 to 800.

2. (Currently Amended) a process according to claim 1 wherin the MFI-~~type~~ crystalline silicate catalyst comprises silicalite.

3. (Currently Amended) a process according to claim 1 wherein the carbon containing~~hydrocarbon~~ feedstock contains at least one hetero compound selected from the group consisting of methanol, ethanol, dimethyl ether, diethyl ether and mixtures thereof.

4. (Currently Amended) A process according to claim 1, wherein the carbon containing~~hydrocarbon~~ feedstock is passed over the crystalline silicate at a reactor inlet temperature of 350 to 650° C.

5. (Currently Amended) A process according to claim 4 wherein the carbon containing~~hydrocarbon~~ feedstock is passed over the crystalline silicate at a reactor inlet temperature of from 450 to 550° C.

6. (Currently Amended) A process according to claim 1 wherein the carbon containing~~hydrocarbon~~ feedstock is passed over the crystalline silicate at a WHSV of from 0.5 to 30 h^{-1}, the WHSV being based on the weight of the at least one C_1 to C_6 aliphatic hetero compound in the feedstock.

7. (Original) A process according to claim 6 wherein the partial pressure of the at least on C_1 to C_6 aliphatic hetero compound in the feedstock when passed over the crystalline silicate is from 20 to 400 kPa.

8-10. (Cancelled)

11. (Original) A process according to claim 1 wherein the crystalline silicate catalyst is pretreated by subjecting said catalyst to steaming, followed by extracting aluminum from the catalyst by contacting said catalyst with a complexing agent for aluminum to remove aluminum resulting from steaming from the pores of the catalyst framework.

12. (Currently Amended) A process according to claim 1 wherein said catalyst comprises an MFI-~~type~~ crystalline silicate having a silicon/aluminum atomic ratio within the range of 250 to 500.

13. (Currently Amended) The process according to claim 1 wherein said catalyst comprises an MEL crystalline silicate having a silicon/aluminum atomic ratio within the range of 150-8~~1~~00.

14. (Original) A process according to claim 1 wherein pretreatment of said catalyst by steaming reduces tetrahedral aluminum in the crystalline silicate framework of the catalyst and converts the tetrahedral aluminum to octahedral aluminum in the form of amorphous alumina, causing partial obstruction of the pores of the crystalline silicate

framework and said catalyst is treated with a complexing agent for aluminum to remove amorphous alumina from the pores of the crystalline silicate framework.

15. (Currently Amended) A process for converting a carbon containing~~hydrocarbon~~ feedstock to provide an effluent containing light olefins comprising:

(a) treating an MFI-~~type~~ crystalline silicate with steam to de-aluminate said catalyst and increase the silicon/aluminum atomic ratio thereof to a value within the range of 250-500;

(b) providing a reactor containing said de-aluminated MFI-~~type~~ crystalline silicate;

(c) supplying a ~~hydrocarbon~~ feedstock containing carbon containing compounds consisting essentially of ~~at least one~~ C_1- C_6 aliphatic hetero compound selected from the group consisting of alcohols, ethers, carbonyl compounds and mixtures thereof to said reactor containing said MFI-~~type~~ crystalline silicate catalyst;

(d) providing steam to said reactor in an amount of up to 80 weight % of said feedstock to said reactor;

(e) operating said reactor under conversion conditions to convert at least a portion of said feedstock to propylene; and

(f) recovering a conversion product containing propylene from said reactor.

16. (Currently Amended) A process according to claim 15 wherein the carbon containing~~hydrocarbon~~ feedstock contains at least one hetero compound selected from the group consisting of methanol, ethanol, dimethyl ether, diethyl ether and mixtures thereof.

17. (Original) The process of claim 15 wherein said feedstock comprises methanol and said reactor is operated under conversion conditions comprising an inlet temperature within the range of 450-550° C.

18. (Original) The process of claim 17 wherein said reactor is operated under conversion conditions providing a product containing propylene and ethylene and having

a propylene/ethylene ratio which is greater than the propylene/ethylene ratio of a conversion product produced by the conversion of a methanol-containing feedstock operated at an inlet temperature in said reactor of 4000 C.

19. (Original) The process of claim 17 wherein said reactor is operated under conversion conditions providing a product containing propylene and propane and having a propylene/propane ratio which is greater than the propylene/propane ratio of a conversion product produced by the conversion of a methanol-containing feedstock operated at an inlet temperature of 4000 C.

20. (Original) A process according to claim 15 wherein pretreatment of said catalyst by steaming reduces tetrahedral aluminum in the crystalline silicate framework of the catalyst and converts the tetrahedral aluminum to octahedral aluminum in the form of amorphous alumina, causing partial obstruction of the pores of the crystalline silicate framework and said catalyst is treated with a complexing agent for aluminum to remove amorphous alumina from the pores of the crystalline silicate framework.

21. (Currently Amended) A process according to claim 15 wherein the carbon containing~~hydrocarbon~~ feedstock is passed over the crystalline silicate at a reactor inlet temperature of from 450 to 550° C.

22. (Currently Amended) A process according to claim 15 wherein the carbon containing~~hydrocarbon~~ feedstock is passed over the crystalline silicate at a WHSV of from 0.5 to 30 h^{-1}, the WHSV being based on the weight of the at least one C_1 to C_6 aliphatic hetero compound in the feedstock.